

Thermodynamic Properties of Liquid Toluene from Speed-of-Sound Measurements at Temperatures from 283.15 to 473.15 K and at Pressures up to 390 MPa

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Abstract

We report the speeds of sound in liquid toluene (methylbenzene) measured using double-path pulse-echo apparatus independently at The University of Western Australia (UWA) and Imperial College London (ICL). The UWA data were measured at temperatures between (306 and 423) K and at pressures up to 65 MPa with standard uncertainties of between (0.02 and 0.04) %. At ICL, measurements were made at temperatures between (283.15 and 473.15) K and at pressures up to 390 MPa with standard uncertainty of 0.06 %. By means of thermodynamic integration, the measured sound-speed data were combined with initial density and isobaric heat capacity values obtained from extrapolated experimental data to derive a comprehensive set of thermodynamic properties of liquid toluene over the full measurement range. Extensive uncertainty analysis was performed by studying the response of derived properties to constant and dynamic perturbations of the sound-speed surface, as well as the initial density and heat capacity values. The relative expanded uncertainties at 95 % confidence of derived density, isobaric heat capacity, isobaric expansivity, isochoric heat capacity, isothermal compressibility, isentropic compressibility, thermal pressure coefficient and internal pressure were estimated to be (0.2, 2.2, 1.0, 2.6, 0.6, 0.2, 1.0 and 2.7) %, respectively. Due to their low uncertainty, these data and derived properties should be well-suited for developing a new and improved fundamental Helmholtz equation of state for toluene.

Keywords

Toluene; Speed of Sound; Thermodynamics; Derived thermodynamic properties; Uncertainty Analysis

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N/A

1. Introduction

Toluene (methylbenzene, C_7H_8) is predominantly used in the production of paints, rubbers, glues and adhesives. It is also a widely-used solvent, a precursor in explosives manufacture, and a component of high-octane gasolines [1]. Toluene can be obtained with high purity, has relatively low toxicity and corrosivity, and exists in the liquid state over a wide range of temperature, making it suitable as a calibration fluid in measurements of thermophysical properties [2].

The use of toluene in various applications depends on the reliability of models to predict its thermodynamic properties over a wide range of temperature and pressure. Such predictions are best made using fundamental equations of state (EOS) [3]. Several EOS models have been developed for toluene. The most widely used is the Helmholtz EOS developed by Lemmon and Span [3], which is valid over a temperature range of (178 to 700) K and pressures up to 500 MPa. The development of equations of state for any fluid requires accurate experimental data for a range of thermodynamic properties, including the speed of sound. The speed of sound in liquid toluene has been reported by several investigators (**Table 1**). The distribution of the literature data in (T, p) -space is provided in **Fig. 1** along with the phase boundary curve.

Table 1. Summary of literature of experimental speed of sound data of toluene.

Reference	Year	N^*	Method	T/K		p/MPa	Uncertainty
Speed of sound at atmospheric pressure and along saturation pressure, p_s							
[4] Freyer	1929	6	SI ^a	273.15	323.15	0.1	1 m/s
[5] Deshpande	1968	3	OI ^b	298.14	318.13	0.1	0.15 %
[6] Zotov	1969	19	PE ^c	293.14	473.15	p_s	2 m/s
[7] Reddy	1986	8	SI	303.14	313.14	0.1	0.1 %
[8] Tamura	1985	3	PE	293.15	303.15	0.1	0.1 %
[9] Gongalez-Olmos	2007	15	PE	288.15	323.15	0.1	1 m/s
[10] Luning Prak	2014	10	PE	293.15	373.15	0.1	1 m/s
[11] Dragoescu	2019	6	PE	298.15	318.15	0.1	0.5 m/s

Speed of sound of compressed liquid phase								
[12] Tagaki	1985	17	PE	303.15		0.1 - 160		0.3%
[13] Muringer	1985	88	PE	173.18	320.30	0.1	263.45	5.1 m/s
[14] Okhotin	1988	150	PE	273.15	473.11	0.1 - 58.93		0.05 %
[15] Vervieko	1991	24	PE	293	373	0.1	250	0.3 %
[16] Meier	2013	222	PE	280	420	0.1	100.17	0.03 %
[17] Yebra	2017	84	PE	283.15	343.15	0.1	95.1	0.1 %
[18] Shchamialiou	2020	36	PE	298.15	433.15	0.1	100.1	0.1 %

^aSonic Interference. ^bOptical Interference. ^cPulse-echo. ^{*}Number of points measured.

It is noteworthy that the most extensive and accurate experimental campaigns were conducted after the development of the Helmholtz EOS by Lemmon and Span [3]. Due in part to the lack of highly-accurate experimental data at the time, the uncertainties in speeds of sound predicted by the EOS 1 % at pressure up to 100 MPa and temperature up to 500 K, increasing to 2 % at higher values of pressure and temperature [3] are considerably larger than the reported standard uncertainties of current data, e.g. well below 0.1 % at pressures up to 100 MPa and temperatures up to 420 K [16].

In this work, we extend both the temperature and pressure ranges at which highly accurate speed-of-sound measurements in liquid toluene have been determined. Based on the measured speeds of sound, we have employed thermodynamic integration to obtain a comprehensive set of thermodynamic properties over the full range of the measurements with small uncertainties. The speeds of sound and derived properties are also compared with available literature data and predictions based on the Helmholtz EOS of Lemmon and Span [3].

2. Experimental Procedure

The sound-speed measurements were carried out using two sets of double-path pulse-echo equipment having different but overlapping operating pressure ranges. At UWA, the apparatus was the same as that used recently by Al Ghafri *et al.* [19] in their study of p-xylene. This apparatus uses a dual-path ultrasonic cell, mounted within a high-pressure stainless-steel vessel, with signal excitation and

detection achieved with a gold-plated piezoelectric ceramic disc transducer operated at 5 MHz. The apparatus was housed in a thermostatic air bath which maintaining temperature stability of better than 0.1 K. Temperature measurements were carried out using platinum resistance thermometer (PRT) probes (Netsushin model NR-141-100S, 1.6 mm diameter) with a standard uncertainty of 0.02 K. Considering the stability of the oven, non-uniformity of temperature across the cell, and the calibration uncertainty, the standard uncertainties in temperature were estimated to be: 0.03 K for $T = (306, 320$ and $343)$ K, 0.04 K for $T = (363$ and $383)$ K, 0.05 K for $T = 403$ K, and 0.07 K for $T = 423$ K. Pressure was measured using a pressure transmitter (Keller model PA-33X) with a full-scale reading of 70 MPa and a manufacturer-specified relative uncertainty of 0.05 % ($k = 1.73$). Its calibration was validated against a hydraulic pressure balance (DH-Budenberg model EHX-580, relative standard uncertainty 0.008 %) and the greatest absolute deviation was found to be 0.019 MPa. Taking this into account, the standard uncertainty of pressure was estimated to be 0.02 MPa within the experimental range. The calibration of the apparatus for this study was carried out using water and has been detailed previously by Al Ghafri *et al.* [19].

The apparatus used at ICL employed a similar 5 MHz double-path pulse-echo apparatus housed in a stainless-steel high-pressure vessel and immersed in a thermostatic oil bath. This apparatus, described in detail by Tay and Trusler [20] had an extended operating temperature ranges of (273.15 to 473.15) K with pressures up to 390 MPa. Pressure was measured with a pressure transducer (Honeywell model TJE/60000) having an estimated standard uncertainty of 0.05 MPa or $6 \cdot 10^{-4} \cdot p$, whichever is greater. Temperature was measured using a PRT (Fluke Model 5615) with a standard uncertainty of 0.015 K. Calibration was carried out with water as a part of the work described earlier [20]. Toluene (methylbenzene) was supplied by Sigma-Aldrich at both UWA and ICL. The sample description is provided in **Table 2**.

Table 2. Description of chemical samples used in the study where w is mass-fraction purity.

Chemical Name	CAS number	Source	Purity w	Purification	Analysis ^a
Toluene ^b	108-88-3	Sigma-Aldrich ^c	0.9993	None	GC
Toluene	108-88-3	Sigma-Aldrich ^d	0.9994	Vacuum degassed	GC

^a Gas-Chromatography. ^b Methylbenzene. ^c Batch Number: SHBG1684V, $w(\text{H}_2\text{O}) = 0.00001$. ^d Lot Number: MKBX7400V, $w(\text{H}_2\text{O}) = 0.00001$.

Experimental uncertainties in the speed of sound arise from the uncertainties in the pressure, temperature, and pulse-echo time delays under both calibration conditions.

the results. At UWA, measurements were also repeated at selected pressures and temperatures to check for the reproducibility of the results when fresh samples were introduced. The relative change in the initial and repeated measurements in all cases were within 0.01 % which confirms that the sensor and the sample were stable during the measurements.

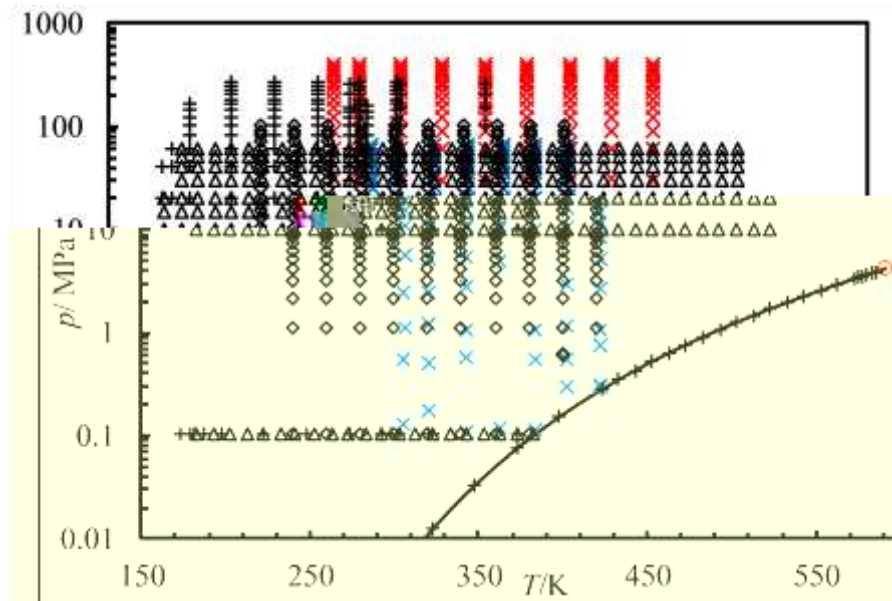


Fig. 1. Selected low uncertainty experimental data of speed-of-sound of liquid Toluene available in literature including experimental data investigated in this work. \times , UWA; \times , ICL; \diamond , Meier *et al.* [16]; \triangle , Okhotin *et al.* [14]; $+$, other experimental data; \circ , Critical point stated by Helmholtz EOS [3]. The solid line represents the liquid-gas phase boundary.

Table 3. Experimental values for the speed of sound of toluene c and standard uncertainty $u(c)$ as a function of pressure p and temperature T measured at UWA.^a

T/K	p/MPa	$c/(\text{m}\cdot\text{s}^{-1})$	$u(c)/(\text{m}\cdot\text{s}^{-1})$
306.17	0.13	1269.90	0.19
306.19	0.53	1272.06	0.19
306.20	1.07	1274.93	0.18
306.16	2.41	1282.21	0.18
306.41	2.43	1279.22	0.18
306.42	4.99	1292.62	0.18
306.24	5.47	1297.90	0.18
306.43	10.58	1320.96	0.18
306.22	10.67	1324.17	0.18
306.43	14.35	1339.30	0.18
306.23	15.10	1345.59	0.18
306.34	16.72	1350.95	0.18
306.23	19.28	1365.11	0.18
306.42	20.29	1367.14	0.18
306.29	24.02	1384.63	0.18
306.31	24.32	1385.92	0.18
306.24	24.84	1390.16	0.18
306.32	25.21	1389.81	0.18
306.28	28.20	1403.11	0.18
306.21	29.77	1411.70	0.18
306.24	29.84	1411.89	0.18
306.10	30.14	1413.70	0.18
306.30	30.40	1412.49	0.18
306.17	32.46	1423.24	0.18

306.30	35.08	1432.10	0.18
306.30	35.11	1432.20	0.18
306.18	41.06	1458.18	0.18
306.18	45.10	1474.01	0.18
306.14	47.84	1484.75	0.18
306.11	51.38	1498.10	0.18
306.17	59.43	1527.36	0.18
306.18	59.78	1528.58	0.18
306.19	64.67	1545.85	0.18

320.45	0.17	1209.59	0.19
320.38	0.49	1211.71	0.19
320.38	1.21	1215.84	0.18
320.38	2.40	1222.63	0.18
320.46	4.04	1223.87	0.18
320.41	5.10	1237.70	0.18
320.46	5.51	1231.91	0.18
320.41	10.40	1266.19	0.18
320.31	10.60	1267.74	0.18
320.31	10.60	1267.74	0.18
320.42	12.73	1269.97	0.18
320.39	19.58	1312.50	0.18
320.55	19.58	1303.15	0.18
320.45	25.92	1332.98	0.17
320.48	26.12	1333.78	0.17
320.45	30.11	1361.11	0.17
320.47	33.53	1376.21	0.17
320.46	39.80	1403.01	0.17

320.42	45.16	1425.21	0.17
320.42	45.16	1425.19	0.17
320.40	49.98	1444.44	0.17
320.40	49.98	1444.44	0.17
320.46	53.00	1456.00	0.17
320.46	53.01	1456.01	0.17
320.42	59.61	1481.06	0.17
320.42	59.61	1481.08	0.17
320.41	65.03	1500.95	0.18
320.41	65.04	1500.98	0.18

343.35	0.11	1114.66	0.19
343.36	0.11	1114.63	0.19
343.37	0.56	1117.55	0.19
343.38	0.57	1117.63	0.19
343.38	1.04	1120.63	0.19
343.38	1.04	1120.69	0.19
343.39	2.72	1131.30	0.19
343.39	2.72	1131.35	0.19
343.42	5.27	1147.11	0.18
343.42	5.27	1147.15	0.18
343.43	10.41	1177.63	0.18
343.43	10.41	1177.65	0.18
343.26	10.94	1181.38	0.18
343.27	10.95	1181.41	0.18
343.44	15.07	1203.83	0.18
343.37	19.36	1227.23	0.18
343.40	25.37	1258.02	0.17

343.41	31.31	1287.05	0.17
343.42	34.92	1303.94	0.17
343.39	44.67	1347.66	0.17
343.40	50.99	1374.36	0.17
343.38	55.43	1392.66	0.17
343.37	58.02	1403.03	0.17
343.37	58.02	1403.06	0.17
343.40	65.05	1430.40	0.17
343.40	65.06	1430.42	0.17
363.18	0.11	1035.00	0.21
363.17	4.86	1068.34	0.20
363.20	9.90	1101.15	0.19
363.20	9.90	1101.21	0.19
363.14	10.88	1107.61	0.19
363.20	19.76	1160.19	0.18
363.20	19.76	1160.17	0.18
363.22	25.13	1189.66	0.18
363.22	30.04	1215.40	0.17
363.21	35.18	1241.19	0.17
363.17	40.05	1264.84	0.17
363.19	44.94	1287.48	0.17
363.19	50.07	1310.39	0.17
363.19	55.18	1332.43	0.17
363.17	60.79	1355.89	0.17
363.15	64.55	1371.16	0.17
363.16	64.58	1371.24	0.17
383.44	0.11	955.06	0.22

383.44	0.55	958.63	0.22
383.45	1.06	962.79	0.22
383.43	9.94	1028.75	0.21
383.44	19.70	1092.02	0.19
383.44	19.71	1092.01	0.19
383.43	24.87	1122.69	0.19
383.39	29.79	1150.45	0.19
383.39	29.79	1150.45	0.19
383.42	35.01	1178.26	0.18
383.42	35.01	1178.27	0.18
383.43	40.28	1205.08	0.18
383.40	44.78	1227.21	0.18
383.40	50.11	1252.28	0.18
383.41	54.92	1274.13	0.18
383.39	59.86	1295.90	0.17
383.35	64.88	1317.23	0.18
383.35	64.88	1317.23	0.18

403.10	0.29	880.19	0.26
403.11	0.55	882.54	0.26
403.07	1.16	888.19	0.26
403.08	2.89	903.45	0.25
403.11	10.08	961.23	0.24
403.06	16.11	1004.91	0.22
403.10	20.06	1031.25	0.22
403.10	20.06	1031.30	0.22
403.04	29.68	1090.66	0.20
403.05	29.69	1090.72	0.20

403.05	34.85	1120.01	0.20
403.05	34.85	1119.99	0.20
403.05	39.99	1147.76	0.19
403.05	39.99	1147.75	0.19
403.06	44.29	1169.94	0.19
403.06	44.29	1169.99	0.19
403.08	50.60	1201.06	0.19
403.06	54.84	1221.20	0.19
403.04	59.96	1244.64	0.19
403.04	64.55	1265.03	0.19

422.63	0.30	804.97	0.32
422.63	0.30	804.99	0.32
422.65	0.73	809.37	0.32
422.65	0.73	809.39	0.32
422.62	1.04	812.59	0.31
422.63	1.04	812.62	0.31
422.63	2.69	828.98	0.31
422.63	2.69	829.04	0.30
422.66	5.08	851.58	0.30
422.57	8.28	880.24	0.28
422.58	8.28	880.28	0.28
422.55	11.28	905.36	0.27
422.54	11.28	905.37	0.26
422.60	14.92	933.70	0.25
422.61	14.93	933.79	0.26
422.63	20.87	976.80	0.24
422.63	20.87	976.83	0.25

422.62	24.86	1003.67	0.24
422.62	24.86	1003.66	0.24
422.65	31.56	1045.82	0.23
422.65	31.56	1045.85	0.23
422.63	34.90	1065.74	0.22
422.63	34.90	1065.72	0.22
422.60	39.92	1094.35	0.22
422.60	39.93	1094.36	0.22
422.59	44.96	1121.61	0.21
422.60	44.97	1121.68	0.21
422.58	50.05	1148.00	0.21
422.58	50.05	1147.99	0.21
422.58	54.88	1171.98	0.21
422.58	54.88	1171.99	0.21
422.59	59.89	1195.82	0.20
422.59	59.90	1195.85	0.21
422.75	64.29	1215.66	0.21

^a Standard uncertainty of temperature $u(T)$: 0.03 K for $T = (306, 320, \text{ and } 343)$ K; 0.04 K for $T = (363 \text{ and } 383)$ K; 0.05 K for $T = 403$ K; 0.07 K for $T = 423$ K. Standard uncertainty of pressure, $u(p) = 0.02$ MPa.

Table 4. Experimental values for the speed of sound of toluene c and standard uncertainty $u(c)$ as a function of pressure p and temperature T measured at ICL.^a

T/K	p/MPa	$c/(\text{m}\cdot\text{s}^{-1})$	$u(c)/(\text{m}\cdot\text{s}^{-1})$
283.15	30.19	1502.39	0.90
283.15	60.14	1609.63	0.97
283.15	90.04	1703.20	1.02
283.15	120.24	1787.54	1.07
283.15	149.99	1863.04	1.12
283.15	180.43	1934.00	1.16
283.15	210.03	1997.94	1.20
283.15	240.31	2059.12	1.24
283.15	269.98	2115.45	1.27
283.15	300.05	2169.82	1.30
283.15	330.05	2221.18	1.33
283.15	360.25	2270.54	1.36
283.15	389.98	2317.01	1.39
298.15	30.08	1443.49	0.87
298.15	60.20	1557.01	0.93
298.15	90.13	1654.39	0.99
298.15	119.97	1740.39	1.04
298.15	150.23	1819.34	1.09
298.15	180.19	1891.02	1.13
298.15	210.16	1957.36	1.17
298.15	240.26	2019.46	1.21
298.15	270.46	2078.03	1.25
298.15	300.15	2132.53	1.28
298.15	329.91	2184.37	1.31

298.15	360.02	2234.29	1.34
298.15	390.01	2282.09	1.37
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323.15	30.00	1350.79	0.81
323.15	60.17	1473.56	0.88
323.15	90.20	1577.76	0.95
323.15	120.66	1670.01	1.00
323.15	150.27	1750.52	1.05
323.15	179.98	1824.20	1.09
323.15	210.22	1893.85	1.14
323.15	240.02	1957.41	1.17
323.15	270.09	2017.64	1.21
323.15	300.07	2074.27	1.24
323.15	330.00	2127.69	1.28
323.15	360.29	2179.26	1.31
323.15	389.93	2227.48	1.34
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348.15	30.15	1265.36	0.76
348.15	60.13	1395.96	0.84
348.15	90.31	1506.73	0.90
348.15	120.32	1602.26	0.96
348.15	150.46	1687.69	1.01
348.15	180.23	1764.23	1.06
348.15	210.54	1836.00	1.10
348.15	240.10	1900.99	1.14
348.15	270.60	1963.70	1.18
348.15	300.32	2021.20	1.21
348.15	330.13	2075.74	1.25
348.15	360.14	2127.73	1.28

348.15	390.00	2176.92	1.31
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373.15	30.07	1183.47	0.71
373.15	60.00	1323.42	0.79
373.15	90.34	1440.60	0.86
373.15	120.24	1540.23	0.92
373.15	150.34	1628.84	0.98
373.15	180.20	1708.20	1.02
373.15	210.11	1781.11	1.07
373.15	240.27	1849.24	1.11
373.15	270.18	1912.25	1.15
373.15	300.19	1971.49	1.18
373.15	330.35	2027.37	1.22
373.15	360.55	2080.74	1.25
373.15	390.03	2130.48	1.28
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398.15	30.07	1107.29	0.66
398.15	60.01	1256.71	0.75
398.15	90.31	1379.44	0.83
398.15	120.39	1483.63	0.89
398.15	150.32	1574.92	0.94
398.15	180.22	1656.81	0.99
398.15	210.00	1731.10	1.04
398.15	240.20	1800.46	1.08
398.15	270.09	1864.90	1.12
398.15	300.00	1925.01	1.16
398.15	330.09	1982.29	1.19
398.15	360.01	2036.20	1.22
398.15	390.00	2088.55	1.25
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423.15	30.08	1035.61	0.62
423.15	60.12	1194.96	0.72
423.15	90.12	1322.02	0.79
423.15	120.03	1429.30	0.86
423.15	150.23	1524.26	0.91
423.15	180.33	1608.84	0.97
423.15	210.09	1684.92	1.01
423.15	240.21	1755.96	1.05
423.15	270.10	1821.45	1.09
423.15	300.10	1883.03	1.13
423.15	329.96	1940.82	1.16
423.15	360.00	1997.13	1.20
423.15	390.00	2049.64	1.23
448.15	30.30	969.48	0.58
448.15	59.95	1136.31	0.68
448.15	90.25	1269.95	0.76
448.15	119.95	1379.82	0.83
448.15	150.22	1477.59	0.89
448.15	180.07	1563.71	0.94
448.15	209.85	1641.64	0.98
448.15	240.09	1714.35	1.03
448.15	270.23	1781.81	1.07
448.15	300.00	1844.24	1.11
448.15	330.05	1904.07	1.14
448.15	360.26	1960.61	1.18
448.15	389.97	2013.46	1.21
473.15	30.06	903.93	0.54

473.15	60.11	1082.96	0.65
473.15	90.33	1221.13	0.73
473.15	120.36	1335.44	0.80
473.15	150.13	1434.05	0.86
473.15	180.09	1522.51	0.91
473.15	210.21	1603.20	0.96
473.15	240.00	1676.68	1.01
473.15	269.85	1745.42	1.05
473.15	300.11	1810.67	1.09
473.15	330.02	1869.02	1.12
473.15	360.02	1926.03	1.16
473.15	390.03	1979.82	1.19

^a Standard uncertainties are $u(T) = 0.015$ K and $u(p) = \text{Max}(0.025 \text{ MPa}, 0.0006 \cdot p)$.

4. Correlation of Data

In order to facilitate comparison with the existing literature and equation-of-state predictions, the measured speed-of-sound data were combined and correlated as a function of pressure and temperature. The thermodynamic integration procedure, discussed later, also depends on the accurate correlation of the speed of sound data over the experimental range. The data were correlated in terms of the following equations:

$$— \tag{1}$$

$$— . \tag{2}$$

Here, $p_0 = 0.1$ MPa is a reference pressure, $c_{0,T}$ is the speed of sound at temperature T and pressure p_0 , and a_{ij} and b_j are parameters which were adjusted to minimise the residual sum of squares. The coefficients are provided in **Table 5**. The values of the coefficients in **Table 5** have been truncated to six decimal places for convenience, beyond which the results obtained from the fit were found to vary insignificantly. For instance, the maximum deviation between the truncated coefficients and actual coefficients upon which the results presented in this study are based was less than 0.5 parts per million. The goodness of fit of the speed-of-sound surface correlation was quantified by analysing the Average Absolute Relative Deviations (AARD) and Maximum Absolute Relative Deviation (MARD).

The experimental speeds of sound from UWA and ICL are compared with the correlation in **Fig. 2** and **Fig. 3**, while the relative deviations are shown in **Fig. 4**. The goodness of fit metrics are $AARD = 0.01$ %, $MARD = 0.08$ % (found at $T = 373.15$ K and $p = 60$ MPa) and the 95 % confidence interval of the average deviations is between (0.012 and 0.016) %. Approximately 85 % of the experimental data set is fitted with absolute deviations of 0.02 %, while 96 % of the data set is fitted with absolute deviations of 0.03.

Table 5. Coefficients of fit of correlations of Eq. (1) and Eq. (2).

a_{10}	-1.148868×10^{-1}	a_{11}	1.061382×10^{-1}	a_{12}	4.474984×10^{-1}	a_{13}	-2.496091×10^{-1}
a_{20}	-4.373371×10^{-4}	a_{21}	1.736190×10^{-3}	a_{22}	-1.812275×10^{-3}	a_{23}	6.885332×10^{-4}
a_{30}	1.208315×10^{-7}	a_{31}	-3.691194×10^{-7}	a_{32}	5.146784×10^{-7}	a_{33}	-2.289112×10^{-7}
b_0	2.958112×10^3	b_1	-2.146336×10^3	b_2	5.986051×10^3	b_3	-1.140723×10^2

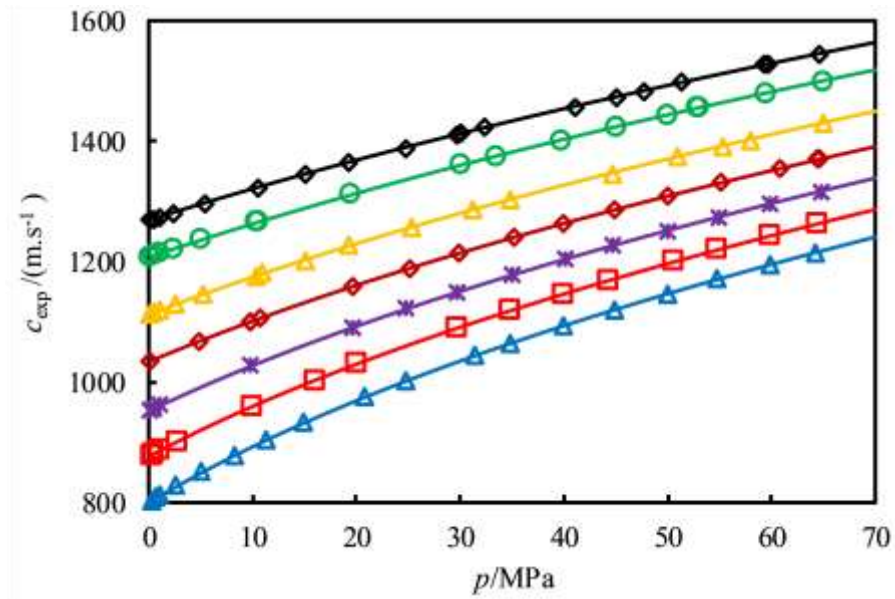


Fig. 2. Experimental speed of sound, c_{exp} , in liquid toluene as a function of pressure measured at UWA. \blacklozenge , $T = 306.19$ K; \bullet , $T = 320.41$ K; \blacktriangle , $T = 343.38$ K; \blacklozenge , $T = 363.19$ K; $*$, $T = 383.41$ K; \blacksquare , $T = 403.07$ K; \blacktriangle , $T = 422.62$ K. Lines represent the values evaluated from the correlation of **Eq. (1)** and **Eq. (2)**.

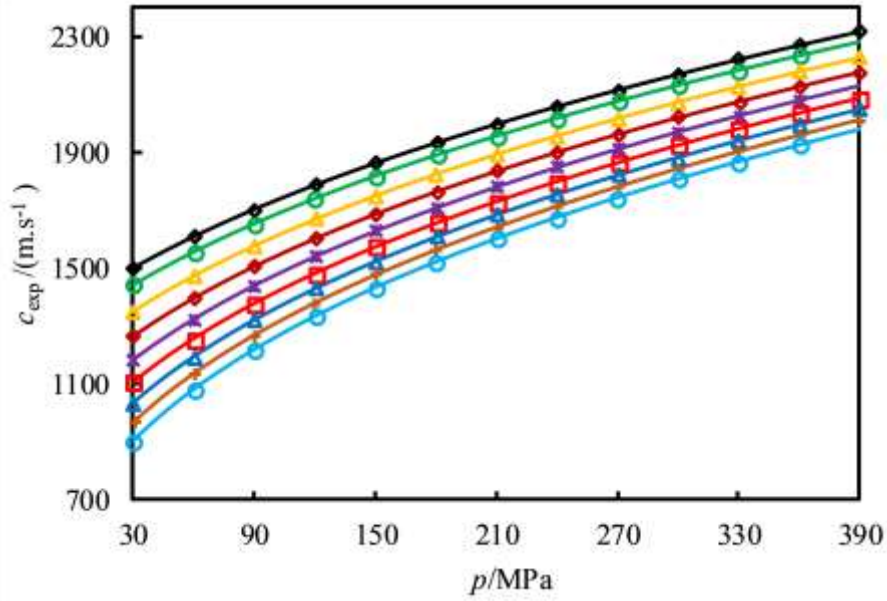


Fig. 3. Experimental speed of sound, c_{exp} , in liquid toluene as a function of pressure measured at ICL. \diamond , $T = 283.15$ K; \circ , $T = 298.15$ K; \triangle , $T = 323.15$ K; \diamond , $T = 348.15$ K; $*$, $T = 373.15$ K; \square , $T = 398.15$ K; \triangle , $T = 423.15$ K; $+$, $T = 448.15$ K; \circ , $T = 473.15$ K. Lines represent the values evaluated from the correlation of **Eq. (1)** and **Eq. (2)**.

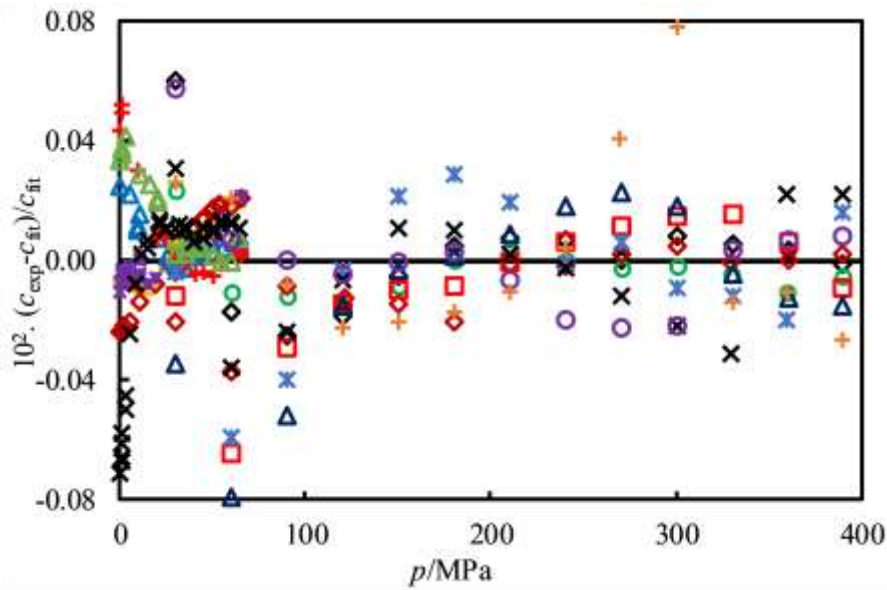


Fig. 4. Relative percentage deviations of the combined experimental speed of sound data measured at UWA and ICL, c_{exp} , from the combined surface fit, c_{fit} , values calculated by using **Eq. (1)** and **Eq. (2)**. \diamond , $T = 283.15$ K; \circ , $T = 298.15$ K; \triangle , $T = 323.15$ K; \diamond , $T = 321.42$ K; $*$, $T = 343.38$ K; \square , $T = 348.15$ K; \triangle , $T = 363.19$ K; \triangle , $T = 373.15$ K; $+$, $T = 383.41$ K; $*$, $T = 398.15$ K; \triangle , $T = 403.04$ K; \times , $T = 422.76$ K; \circ , $T = 448.15$ K; $+$, $T = 473.15$ K.

5. Comparison of speed of sound with literature data

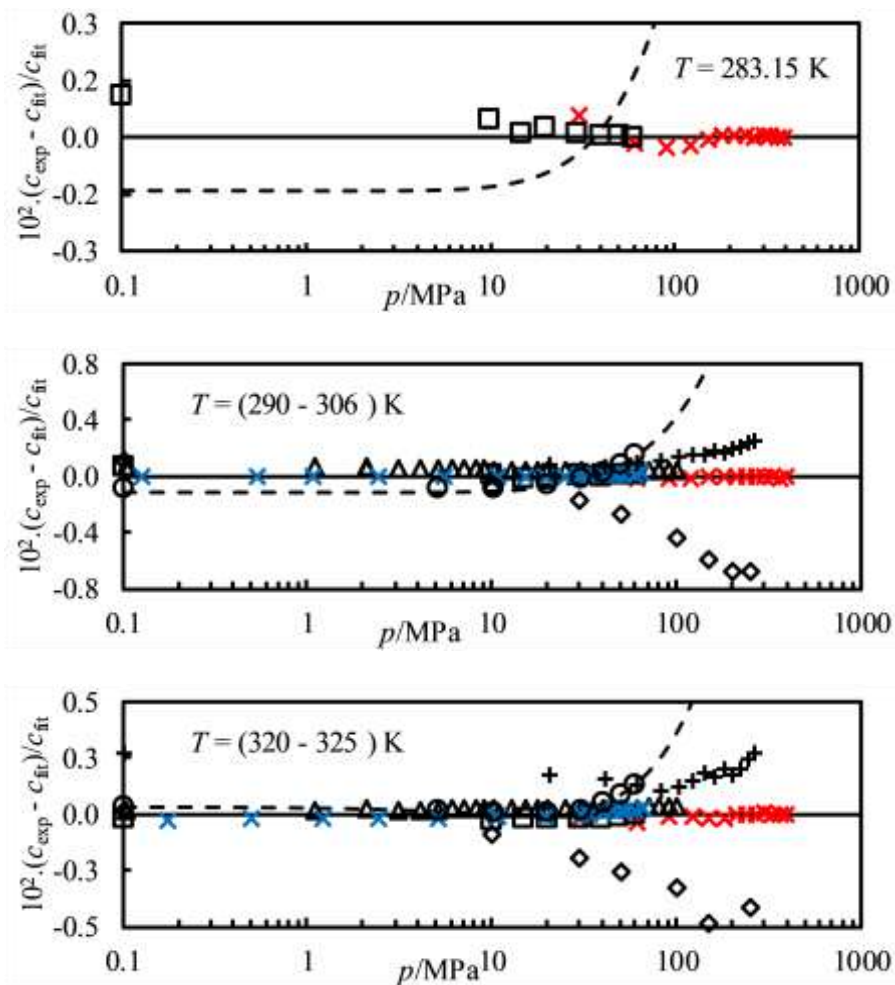
In this section, our sound-speed data are compared against the Helmholtz EOS model of Lemmon and Span [3] as well as the most accurate experimental data currently available for toluene in the investigated region. The relative deviations of the EOS and literature experimental data from the surface-fit correlated to our data (which is chosen as the baseline) are plotted against pressures at various experimental isotherms used in this study as shown in **Fig. 5** and **Fig. 6**.

At pressures up to 100 MPa and at all temperatures, the Helmholtz EOS of Lemmon and Span [3] represents our data to within its reported standard uncertainty of 1 % in that range. At higher pressures, the values obtained from EOS vary from our correlation by up to 2.1 % which is close to the reported EOS uncertainty of 2 %. The deviations are the greatest at the highest pressures of the isotherms $T = (373.15 \text{ and } 383.41) \text{ K}$. The maximum and average deviations of the EOS from our correlation are summarized in **Table S1** of the supplementary information section.

Comparisons were also made against other EOS models, but have not been presented graphically owing to their very high deviations from the available literature and our experimental data. In summary, the EOS of Polt *et al.* [21] within the range of its validity of up to 25 MPa in pressure deviates from our data by up to nearly 2 % at the highest pressures along all isotherms. At higher pressures, for all temperatures, their EOS always overestimates our data with the deviations increasing with increasing pressure. Similarly, the non-analytical EOS of Goodwin [22] at selected pressures follows a similar trend. However, it consistently overestimates the data at lowest pressures with deviations of up to 5 % at the lowest isotherm and lowest pressures. At other points of pressure and temperature, the deviations fall within 2 %.

Our correlated data most closely and consistently agree with the experimental data of Meier *et al.* [16]. Most of the deviations are within the reported expanded uncertainty of their data of 0.03 %. Deviations of up to 0.06 % from their data occur at the lowest pressures at $T = 300 \text{ K}$. The data from Okhotin *et al.* [14] also show close agreement with our data with most of the deviations falling within the reported experimental uncertainty of 0.05 % with average deviations below 0.03 % for all isotherms. However, larger deviations of up to 0.12 % are observed at $p = 0.1 \text{ MPa}$ at $T = 383.12 \text{ K}$, which is close to the normal boiling point of $T = 383.75 \text{ K}$. The data from Vervieko *et al.* [15] at $T = (293, 323 \text{ and } 373) \text{ K}$

are consistently lower than our data at all pressures, except at $p = 0.1$ MPa. The highest deviations of up to 0.7 % occur at their highest reported pressure of $p = 250$ MPa. Similarly, the data from Muringer *et al.* [13] at $T = (298.14$ and $320.29)$ K are consistently close to 0.2 % higher than our data with the highest deviation of 0.3 % occurring at the atmospheric pressure, $p = 0.1$ MPa. The 2017 data by Yebra *et al.* [17] at $T = (303.15, 323.15$ and $343.15)$ K have average deviations of close to 0.1 % from our data. However, at the highest pressure of $p = 60.1$ MPa and at atmospheric pressures, deviations of up to 0.2 % are observed.



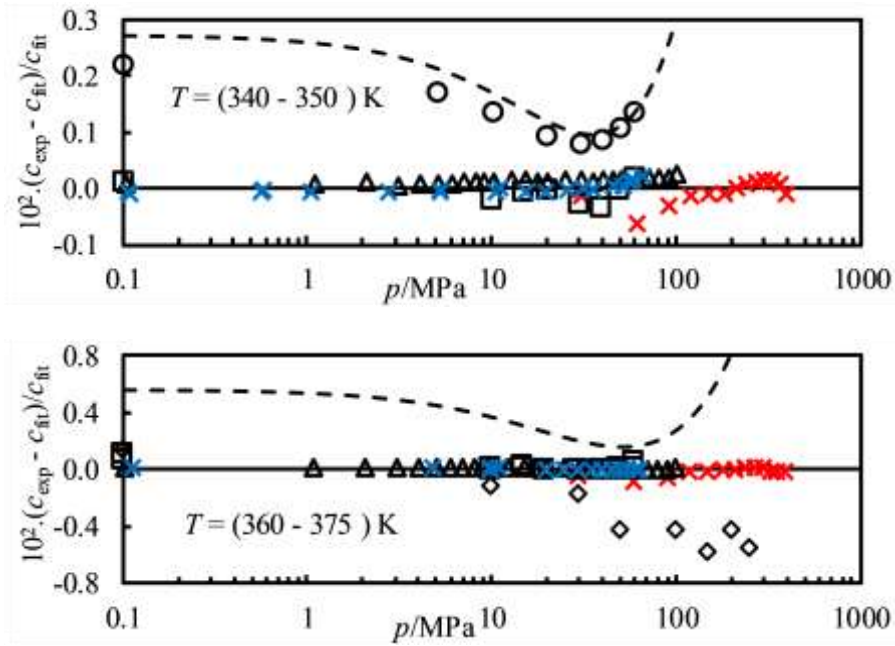
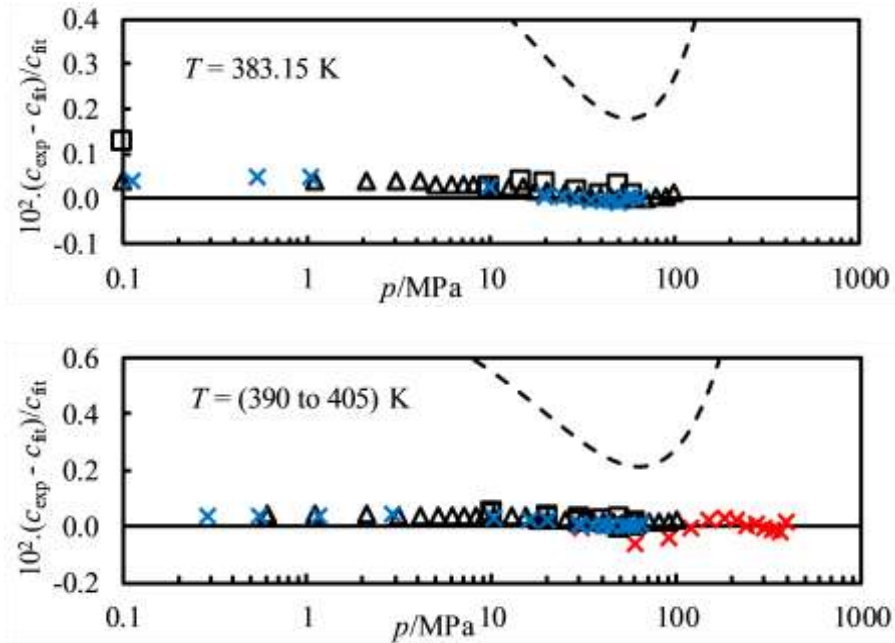


Fig. 5. Relative percentage deviations for experimental literature data (c_{exp} , symbols) and the Helmholtz EOS [3] (dotted lines), calculated relative to the surface-fit correlation of this work (baseline), c_{fit} . Deviations are presented as a function of pressure at temperatures in the vicinity of the experimental isotherms used in this work. Experimental data: \times , UWA; \times , ICL; Δ , Meier *et al.* [16] at 300 K, 320 K, 340 K and 360 K; \circ , Yebra *et al.* [17] at 303.15 K, 323.15 K and 343.15 K; \diamond , Vervieko *et al.* [15] at 323 K and 373 K; $+$, Muringer *et al.* [13] at 298.14 K and 320.29 K and \square , Okhotin *et al.* [14] at 283.19 K, 293.15 K, 323.14 K, 343.14 K, 363.12 K and 373.12 K. EOS: \blacksquare , Lemmon and Span [3].



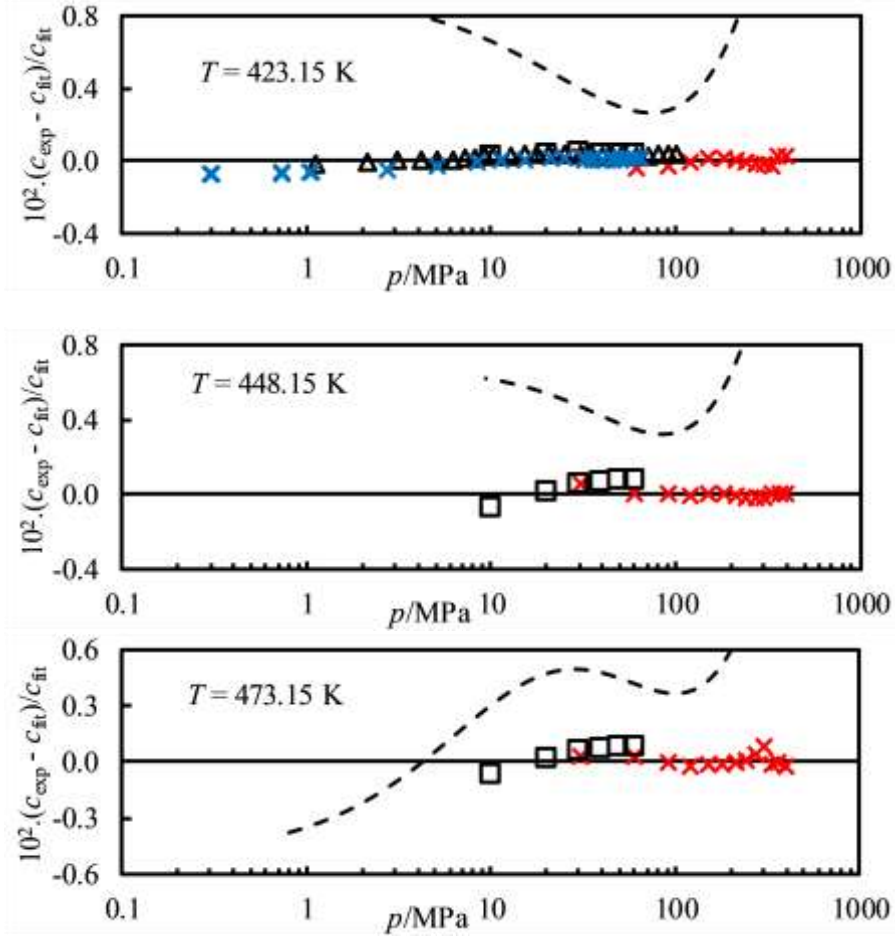


Fig. 6. Relative percentage deviations for experimental literature data (c_{exp} , symbols) and the Helmholtz EOS [3] (dotted lines), calculated relative to the surface-fit correlation of this work (baseline), c_{fit} . Deviations are presented as a function of pressure at temperatures in the vicinity of the experimental isotherms used in this work. Experimental data: \times , UWA; \times , ICL; Δ , Meier *et al.* [16] at 380 K, 400 K and 420 K and \square , Okhotin *et al.* [14] at 383.12 K, 393.12 K, 403.12 K, 423.11 K, 443.11 K and 473.11 K. EOS: \square , Lemmon and Span [3].

6. Derived thermodynamic properties and uncertainties

Thermodynamic properties over the investigated ranges of temperature and pressure can be derived with very high accuracy from the sound-speed surface by means of numerical integration of the following partial differential equations (PDEs):

$$\begin{aligned} & \frac{\partial \ln \rho}{\partial \ln p} = \frac{1}{\gamma} \left(\frac{\partial \ln \rho}{\partial \ln T} + \frac{\partial \ln \rho}{\partial \ln p} \right) \\ & \frac{\partial \ln \rho}{\partial \ln T} = \frac{1}{\gamma} \left(\frac{\partial \ln \rho}{\partial \ln T} + \frac{\partial \ln \rho}{\partial \ln p} \right) \end{aligned} \quad (3)$$

The solutions of these PDEs are subject to prescribed initial values of density and specific heat capacity along the isobar at $p = p_0 = 0.1$ MPa. For the initial densities, a correlation was created by first

extrapolating the low uncertainty experimental data of McLinden & Splett [23] and Tay & Trusler [20] to p_0 and then correlating the results in terms of the equation:

$$\text{---} \quad , \quad (4)$$

with coefficients d_j and exponents e_j as adjustable parameters. The data were weighted based on the experimental uncertainties and optimum solution was obtained by minimizing the weighted residual sum of squares. Similarly, a third-order polynomial fit was used to correlate the isobaric heat capacity in a similar way, based on the experimental data of Akhundov *et al.* [24], Chirico & Steele [25], Cerdeiriña *et al.* [26] and Perderson *et al.* [27] and in terms of the equation:

$$\text{---} \quad (5)$$

with coefficients g_j as an adjustable parameter. The values at high pressures were extrapolated to $p = p_0$, while those pertaining to saturation condition were corrected to the (possibly hypothetical) state at $p = p_0$ with the help of the EOS of Lemmon and Span [3]. The coefficients of the correlations of **Eq. (4)** and **Eq. (5)** are provided in **Table 6**.

Table 6

Coefficients of fit of correlations of **Eq. (4)**^a and **Eq. (5)**^b for various reference pressures.

j	d_j	e_j	g_j
0	-	-	1.054785
1	1.123743×10^3	0.000	0.517658
2	-8.354357×10^1	1.042	0.036530
3	-1.600587×10^{-4}	7.765	0.105107

Weighted Sum of Squares of Errors: ^aWSSQ = 0.043. ^bWSSQ = 0.0045.

The PDEs, **Eq. (3)**, were integrated using a predictor-corrector algorithm implemented in MATLAB. Prediction of the density, ρ , and isobaric heat capacity, C_p , at each temperature and pressure grid-point was carried out by first-order Taylor series expansion and the predicted values were corrected by using a more accurate mid-point formula as employed by Davila and Trusler [28]. Temperature-derivatives

of ρ and C_p at each grid-point were obtained by means of third-order polynomial fitting which was found to sufficiently represent the calculated data. Rigorous mesh-dependency tests were carried out to ensure that the algorithm implemented was insensitive to the grid of spacings defined by $(\Delta T, \Delta p)$. Trial step sizes for temperature were $\Delta T = (10, 5, 2.5 \text{ and } 1) \text{ K}$. The differences in the derived densities for all trial grids were less than 9 ppm overall with convergence as the grid size were lowered. The difference between 2.5 K and 1 K grid sizes for density results was less than 3 ppm along all isobars and isotherms. The results in isobaric heat capacity showed similar behaviour with the maximum difference in values between temperature-grids of 2.5 K and 1 K being less than 70 ppm. Therefore, $\Delta T = 1 \text{ K}$ was chosen as the final temperature grid-size. Similarly, step sizes for pressure were varied between $\Delta p = (0.1 \text{ and } 0.01) \text{ MPa}$ with resulting variation in density of less than 0.07 ppm and isobaric heat capacity of less than 0.25 ppm throughout the whole range of integration. Finally, the pressure grid-size of $\Delta p = 0.1 \text{ MPa}$ was chosen for computational efficiency. Since these variations are much less than the typical uncertainties of the most accurate available data for density and isobaric heat capacity of toluene i.e. 500 ppm and 5000 ppm respectively, it can be concluded that the chosen step sizes of pressure and temperature render the numerical error in the integration algorithm negligible. These results suggest that the implemented algorithm is mesh-independent within the allowable limits of uncertainties.

The accuracy of the derived thermodynamic properties is dependent upon the speed-of-sound surface employed as well as the initial values of density and heat capacities imposed along the isobar at $p = p_0$. However, the evaluation of uncertainties of the derived properties obtained from the thermodynamic integration of sound-speed data is a non-trivial problem. The typical way of estimating these uncertainties is to study empirically the effect on the derived properties of variation of input parameters by a fixed percentage. Trusler and Lemmon [29] advocated a more comprehensive strategy in which these parameters are subject to both constant and oscillatory perturbations. In the remainder of this section, a brief description of the methodology is provided its application in this work is explained. Here, we follow the same methodology detailed in [29] with the only difference being in the way in which the temperature derivatives are calculated.

Defining an arbitrary dimensionless number $\epsilon \ll 1$ and a function f_1 of the order of unity, the perturbed speed of sound c related to the true speed of sound by:

$$c = c_0 (1 + \epsilon f_1) \quad (6)$$

Similarly, the perturbed values of ρ and C_p can be stated as follows:

$$\rho = \rho_0 (1 + \epsilon f_2) \quad (7)$$

$$C_p = C_{p0} (1 + \epsilon f_3) \quad (8)$$

Substitution of the perturbed quantities in **Eq. (3)** and isolation of the first-order terms in ϵ leads to the following auxiliary PDEs:

$$\begin{aligned} \frac{\partial^2 f_1}{\partial x^2} + \frac{\partial^2 f_1}{\partial y^2} + \frac{\partial^2 f_1}{\partial z^2} - \frac{1}{c_0^2} \frac{\partial^2 f_1}{\partial t^2} &= -\frac{1}{c_0^2} \frac{\partial^2 f_1}{\partial t^2} \quad (9) \\ \frac{\partial^2 f_2}{\partial x^2} + \frac{\partial^2 f_2}{\partial y^2} + \frac{\partial^2 f_2}{\partial z^2} - \frac{1}{c_0^2} \frac{\partial^2 f_2}{\partial t^2} &= -\frac{1}{c_0^2} \frac{\partial^2 f_2}{\partial t^2} \end{aligned}$$

where,

$$\frac{\partial^2 f_3}{\partial x^2} + \frac{\partial^2 f_3}{\partial y^2} + \frac{\partial^2 f_3}{\partial z^2} - \frac{1}{c_0^2} \frac{\partial^2 f_3}{\partial t^2} = -\frac{1}{c_0^2} \frac{\partial^2 f_3}{\partial t^2} \quad (10)$$

These auxiliary PDEs relate the functions f_1, f_2 and f_3

$$\dots, \tag{14}$$

where the amplitudes are given by $A_i = 1$ or 0 , according to where the corresponding perturbations are switched on or off. Calculations were carried out for both constant ($k_j = 0$) and dynamic/variable ($k_j > 0$) perturbations.

The resulting absolute error in thermal expansivity can be expressed as:

$$\dots \tag{15}$$

The PDEs of **Eq. (9)** were also implemented in MATLAB and solution was achieved with initial assumed perturbations of $f_1, f_{2,0}$ and $f_{3,0}$ by Trusler and Lemmon [29].

The main difficulty in this method arises during the evaluation of the derivatives of temperature in **Eq. (9)**. Since the dynamic perturbations ($k_j > 0$) we have in this study are sinusoidal in nature, we employed a six-variable second-order sum-of-sine fit to relate the quantities \dots and \dots as functions of temperature along individual isobars. The equation of fit employed is given by:

$$\dots, \tag{16}$$

where X is either \dots and \dots . These fitted quantities were then differentiated with respect to temperature along each isobar.

The choice of order of fit for the dynamic perturbations was made after an extensive analysis of fit at various isobars. The fit coefficients vary at each isobar with the variation in the values of f_2 and \dots . The improvement in sum-of-sine fit from first-order to second-order was found to be significant with the sum of squares of errors more than eight orders of magnitude lower with this increase in order of fit. Hence, the second-order sum-of-sine fit was employed to fit the temperature derivatives of **Eq. (9)**. This higher order fit also ensures that the more rapid fluctuations owing to high k_j values are well explained. In the case of constant perturbations ($k_j = 0$), a second-order polynomial fit was found sufficiently represent the fitted data.

To illustrate the overall nature of dynamic perturbations on the derived properties, k_1 , k_2 and k_3 were selected from values of (0.05, 0.1 and 0.2) K^{-1} , corresponding to wavelengths of about (125, 63 and 31) K, while k_4 was either zero or 0.05 MPa^{-1} . The results of the sensitivity analysis are summarized in **Table 7** which includes various scenarios of constant and dynamic perturbations. A selection of the results is also represented graphically in **Figures S1 to S6** of the **Supplementary Information**.

These results illustrate the negative impact of temperature-dependent fluctuations in any of the input quantities on the derived isobaric heat capacity and isobaric expansivity. When the cyclic variations of sound-speed with pressure are also considered, the perturbations decrease significantly. These observations suggest that the cyclic variation with pressure reduce the negative impact of variations with respect to temperature. Since the effect of f_1 at a given temperature oscillates with increasing pressure and is not constant, the reduction in the effect of sound-speed perturbation on derived property perturbation functions is reasonable. These observations are consistent with those made by Trusler and Lemmon [29].

Constant perturbations of the input parameters have a minimal effect on the derived properties. However, dynamic perturbations in input quantities lead to higher perturbations in derived properties. Particularly, the short wavelength perturbations have the most negative impact on the derived properties with the resulting perturbations being orders of magnitude higher than in the case of slowly varying perturbations in temperature. These observations suggest that fit of sound-speed data needs to be such that these perturbations do not vary rapidly with increasing temperature. The fit deviations in this study do not vary rapidly with temperature.

Following these observations, the uncertainties in derived properties in this study were estimated by considering the average of constant perturbations and dynamic perturbations (cf. **Table 7**, Cases I to V) resulting from the input perturbations equivalent to the experimental uncertainty of the experimental sound-speed data (0.08 %) and the highest uncertainties in initial values of density (0.1 %) and isobaric heat capacity (1 %) from the experimental data that were used for correlations. For an arbitrary derived property, z , the overall standard uncertainty was estimated by:

$$\dots \quad (17)$$

In the above equation, the first term on the right-hand-side describes the influence of overall sound-speed measurement uncertainty on the derived property. Similarly, the second and third terms describe the influence of overall uncertainty of initial density and heat capacities. The uncertainties in density and isobaric heat capacity were estimated by means of constant input perturbations to **Eq. (9)** with the resulting perturbed values given by **Eq. (7)** and **Eq. (8)**. The uncertainties in the other derived properties described in this work were then evaluated by using the perturbed values of speed of sound, density, and isobaric heat capacities over the entire thermodynamic integration range. The overall expanded uncertainties of all derived properties are provided in **Table 8**.

Other thermodynamic properties were also calculated based on the correlated speed of sound and derived density and isobaric heat capacity values. The following relations were used to evaluate isobaric expansivity, α_p and isothermal compressibility, β_T properties of liquid toluene:

$$\dots \quad (18)$$

$$\dots \quad (19)$$

Similarly, a useful relation for the speed of sound propagation which relates the density, heat capacities and isothermal compressibility with isentropic compressibility in fluid phases, β_S , can be used to derive other thermodynamic properties [30]:

$$\dots \quad (20)$$

The thermal pressure coefficient can be obtained as:

$$\dots \quad (21)$$

Finally, the thermodynamic equation of state can be used to evaluate the internal pressure, p_{int} according to the relation:

$$\dots \quad (22)$$

All derived thermodynamic properties with the overall relative uncertainties over a range of selected isobars and isotherms are provided in **Table 8**.

Table 7

Summary of results of sensitivity analysis depicting average and maximum deviations of perturbed quantities from derived quantities as results of constant and dynamic perturbations. The deviations resulting from cases highlighted in bold were averaged and used in **Eq. (17)** to estimate expanded uncertainties of derived properties.

Case	Pert. type	Pert. quantity	Switches			Repetency				Pert. amount, (%)	AARD (%)			MARD (%)		
			A ₁	A ₂	A ₃	k ₁ (K ⁻¹)	k ₂ (K ⁻¹)	k ₃ (K ⁻¹)	k ₄ (MPa ⁻¹)		C _p			C _p		
I	Constant	<i>c</i>	1	0	0	0	0	0	0	0.08	0.01	0.01	0.04	0.01	0.02	0.12
II	Constant	ρ_0	0	1	0	0	0	0	0	0.10	0.09	0.01	0.06	0.10	0.03	0.16
III	Constant	C _{p,0}	0	0	1	0	0	0	0	1.00	0.02	1.01	0.07	0.04	1.09	0.22
IV	Dynamic	<i>c</i>	1	0	0	0.025	0	0	0	0.08	0.01	0.08	0.15	0.01	0.39	0.58
V	Dynamic	<i>c</i>	1	0	0	0.025	0	0	0.03	0.08	0.00	0.03	0.06	0.00	0.15	0.23
VI	Dynamic	<i>c</i>	1	0	0	0.2	0	0	0	0.08	0.01	2.33	2.19	0.08	19.19	19.19
VII	Dynamic	<i>c</i>	1	0	0	0.1	0	0	0.05	0.08	0.00	0.41	0.38	0.02	2.81	1.94
VIII	Dynamic	<i>c</i>	1	0	0	0.2	0	0	0.05	0.08	0.01	2.21	2.25	0.06	20.13	16.19
IX	Dynamic	ρ_0	0	1	0	0	0.05	0	0	0.10	0.09	4.41	6.56	0.20	15.62	20.91
X	Dynamic	C _{p,0}	0	0	1	0	0	0.05	0	1.00	0.01	1.40	1.18	0.04	5.50	5.57

Table 8Derived thermodynamic properties of liquid toluene at isotherms T and selected isobars of pressures p .^a

p/MPa	$c/(\text{m}\cdot\text{s}^{-1})^b$	$(\text{kg}\cdot\text{m}^{-3})$	$C_p/\text{J}\cdot\text{kg}^{-1}\cdot\text{K}^{-1}$	$C_v/\text{J}\cdot\text{kg}^{-1}\cdot\text{K}^{-1}$	$p\cdot 10^6/\text{K}^{-1}$	$T\cdot 10^6/\text{MPa}^{-1}$	$s\cdot 10^6/\text{MPa}^{-1}$	$p_c/\text{MPa}\cdot\text{K}^{-1}$	p_{int}/MPa
$T = 283 \text{ K}$									
0.1	1370.33	876.24	1661.75	1226.14	1053.99	823.66	607.75	1.2796	362.04
10	1417.04	883.19	1656.34	1222.97	1016.30	763.70	563.88	1.3308	366.61
50	1575.68	907.00	1642.04	1244.72	863.70	585.83	444.08	1.4743	367.23
100	1732.91	930.83	1636.94	1265.29	752.17	462.83	357.75	1.6252	359.92
120	1787.71	939.16	1636.99	1272.88	719.54	428.48	333.17	1.6793	355.24
150	1863.61	950.68	1638.39	1283.71	678.65	386.55	302.87	1.7557	346.86
180	1933.38	961.27	1640.91	1293.94	644.94	352.93	278.30	1.8274	337.15
210	1998.16	971.09	1644.20	1303.67	616.53	325.29	257.92	1.8953	326.37
240	2058.78	980.26	1648.04	1312.95	592.16	302.11	240.68	1.9601	314.71
270	2115.88	988.88	1652.28	1321.85	570.95	282.34	225.88	2.0222	302.29
300	2169.94	997.03	1656.81	1330.42	552.29	265.26	213.01	2.0820	289.22
330	2221.35	1004.77	1661.55	1338.69	535.69	250.34	201.70	2.1399	275.58
360	2270.43	1012.14	1666.46	1346.70	520.81	237.17	191.67	2.1959	261.43
390	2317.42	1019.19	1671.49	1354.47	507.35	225.46	182.70	2.2503	246.83
$T = 298 \text{ K}$									
0.1	1304.93	862.33	1708.04	1268.38	1080.15	917.06	681.01	1.1778	350.89
10	1354.51	869.87	1700.89	1270.03	1027.32	839.16	626.59	1.2242	354.82
50	1521.23	895.38	1683.57	1289.89	863.19	629.92	482.62	1.3703	358.36
100	1684.58	920.49	1677.33	1310.63	744.94	489.93	382.82	1.5205	353.11
120	1741.19	929.19	1677.19	1318.31	710.90	451.62	354.98	1.5741	349.09
150	1819.36	941.18	1678.44	1329.26	668.57	405.31	320.99	1.6495	341.56
180	1891.00	952.15	1680.91	1339.63	633.92	368.53	293.71	1.7201	332.60
210	1957.35	962.29	1684.21	1349.49	604.88	338.52	271.24	1.7869	322.48
240	2019.32	971.74	1688.09	1358.93	580.09	313.50	252.37	1.8503	311.40
270	2077.59	980.60	1692.41	1367.98	558.60	292.29	236.26	1.9111	299.51

300	2132.67	988.96	1697.03	1376.71	539.75	274.05	222.32	1.9695	286.92
330	2184.98	996.88	1701.89	1385.13	523.03	258.17	210.12	2.0259	273.72
360	2234.84	1004.42	1706.91	1393.30	508.07	244.21	199.34	2.0805	259.99
390	2282.54	1011.61	1712.06	1401.22	494.59	231.82	189.74	2.1334	245.77
$T = 306 \text{ K}$									
0.1	1270.58	854.86	1732.97	1291.30	1095.38	972.44	724.60	1.1264	344.59
10	1321.88	862.74	1724.76	1294.78	1034.99	883.62	663.34	1.1713	348.42
50	1493.17	889.23	1705.64	1313.86	863.42	654.80	504.39	1.3186	353.49
100	1659.80	915.05	1698.72	1334.67	741.38	504.88	396.68	1.4684	349.33
120	1717.35	923.95	1698.46	1342.38	706.56	464.32	366.97	1.5217	345.64
150	1796.69	936.19	1699.60	1353.39	663.44	415.54	330.90	1.5966	338.55
180	1869.28	947.37	1702.01	1363.82	628.28	377.00	302.09	1.6665	329.96
210	1936.42	957.68	1705.30	1373.75	598.90	345.68	278.47	1.7325	320.16
240	1999.07	967.27	1709.19	1383.26	573.88	319.66	258.70	1.7953	309.36
270	2057.92	976.26	1713.53	1392.39	552.24	297.65	241.87	1.8553	297.73
300	2113.51	984.73	1718.19	1401.18	533.28	278.77	227.34	1.9130	285.37
330	2166.26	992.75	1723.08	1409.68	516.50	262.37	214.65	1.9686	272.38
360	2216.52	1000.38	1728.15	1417.92	501.50	247.98	203.47	2.0223	258.83
390	2264.58	1007.65	1733.34	1425.92	488.00	235.24	193.52	2.0745	244.79
$T = 321 \text{ K}$									
0.1	1207.13	840.73	1780.38	1334.99	1126.89	1088.60	816.27	1.0352	332.19
10	1261.97	849.34	1769.90	1340.65	1052.86	976.01	739.30	1.0787	336.28
50	1442.28	877.78	1747.01	1358.64	864.81	704.22	547.67	1.2280	344.20
100	1615.06	904.97	1738.65	1379.51	735.25	533.92	423.63	1.3771	342.04
120	1674.33	914.26	1738.12	1387.27	698.92	488.84	390.17	1.4297	338.95
150	1755.78	926.98	1739.01	1398.36	654.29	435.18	349.94	1.5035	332.62
180	1830.08	938.55	1741.29	1408.89	618.16	393.18	318.13	1.5722	324.67
210	1898.65	949.19	1744.50	1418.93	588.14	359.31	292.25	1.6369	315.43
240	1962.50	959.06	1748.37	1428.55	562.68	331.34	270.73	1.6982	305.12

270	2022.38	968.29	1752.71	1437.79	540.74	307.81	252.50	1.7567	293.92
300	2078.87	976.97	1757.39	1446.70	521.59	287.71	236.84	1.8129	281.95
330	2132.42	985.18	1762.32	1455.31	504.68	270.31	223.22	1.8670	269.31
360	2183.39	992.97	1767.43	1463.65	489.61	255.10	211.25	1.9193	256.09
390	2232.08	1000.39	1772.68	1471.75	476.06	241.66	200.64	1.9700	242.36

$T = 343 \text{ K}$

0.1	1116.15	819.67	1852.06	1400.67	1181.87	1294.91	979.31	0.9127	312.96
10	1176.94	829.55	1837.48	1407.00	1087.78	1136.53	870.27	0.9571	318.29
50	1371.42	861.17	1808.01	1424.10	869.21	783.84	617.40	1.1089	330.36
100	1553.17	890.50	1797.13	1444.90	727.63	578.99	465.51	1.2567	331.06
120	1614.87	900.38	1796.10	1452.68	688.98	526.57	425.89	1.3084	328.79
150	1699.28	913.84	1796.49	1463.83	642.03	465.09	378.97	1.3804	323.49
180	1775.95	925.99	1798.44	1474.43	604.42	417.64	342.40	1.4472	316.40
210	1846.48	937.12	1801.44	1484.55	573.43	379.79	312.98	1.5099	307.88
240	1911.98	947.40	1805.17	1494.25	547.32	348.82	288.74	1.5691	298.20
270	1973.29	956.98	1809.41	1503.57	524.94	322.94	268.36	1.6255	287.54
300	2031.02	965.97	1814.03	1512.57	505.49	300.98	250.96	1.6795	276.07
330	2085.66	974.45	1818.92	1521.27	488.39	282.07	235.91	1.7314	263.88
360	2137.61	982.48	1824.01	1529.69	473.20	265.61	222.75	1.7816	251.07
390	2187.17	990.13	1829.24	1537.87	459.59	251.13	211.13	1.8301	237.72

$T = 348 \text{ K}$

0.1	1095.79	814.81	1868.79	1415.83	1196.16	1349.08	1022.09	0.8866	308.45
10	1158.06	825.02	1853.14	1421.98	1097.24	1177.84	903.80	0.9316	314.19
50	1355.91	857.43	1821.97	1438.96	870.62	803.22	634.37	1.0839	327.20
100	1539.68	887.26	1810.44	1459.72	726.13	589.66	475.43	1.2314	328.54
120	1601.92	897.29	1809.28	1467.49	686.93	535.45	434.30	1.2829	326.45
150	1686.98	910.91	1809.53	1478.63	639.44	472.08	385.75	1.3545	321.38
180	1764.17	923.20	1811.39	1489.23	601.49	423.33	348.04	1.4209	314.47
210	1835.13	934.43	1814.33	1499.36	570.27	384.53	317.78	1.4830	306.10

240	1900.99	944.81	1818.00	1509.06	544.01	352.84	292.88	1.5418	296.55
270	1962.61	954.48	1822.20	1518.40	521.53	326.42	272.00	1.5977	286.01
300	2020.61	963.54	1826.79	1527.40	502.01	304.02	254.20	1.6512	274.63
330	2075.49	972.08	1831.65	1536.10	484.86	284.76	238.81	1.7027	262.54
360	2127.65	980.17	1836.72	1544.53	469.64	268.01	225.37	1.7524	249.82
390	2177.41	987.86	1841.94	1552.71	456.02	253.29	213.51	1.8004	236.55

$T = 363 \text{ K}$

0.1	1035.38	800.04	1920.18	1461.78	1243.94	1531.61	1165.98	0.8122	294.72
10	1102.41	811.33	1900.91	1466.84	1129.21	1314.31	1014.19	0.8592	301.88
50	1310.60	846.26	1864.18	1483.57	875.80	864.43	687.94	1.0131	317.77
100	1500.42	877.67	1850.53	1504.10	722.19	622.68	506.11	1.1598	321.01
120	1564.25	888.11	1848.93	1511.82	681.29	562.78	460.17	1.2106	319.44
150	1651.22	902.25	1848.71	1522.91	632.14	493.46	406.50	1.2810	315.01
180	1729.93	914.95	1850.23	1533.47	593.14	440.65	365.21	1.3461	308.62
210	1802.14	926.53	1852.91	1543.57	561.24	398.93	332.33	1.4069	300.69
240	1869.06	937.19	1856.39	1553.25	534.52	365.05	305.44	1.4642	291.51
270	1931.59	947.10	1860.43	1562.56	511.73	336.94	282.99	1.5187	281.30
300	1990.39	956.37	1864.88	1571.53	492.00	313.20	263.94	1.5709	270.22
330	2045.98	965.10	1869.62	1580.21	474.70	292.86	247.53	1.6209	258.39
360	2098.77	973.35	1874.59	1588.62	459.39	275.22	233.24	1.6692	245.91
390	2149.11	981.19	1879.71	1596.77	445.72	259.77	220.66	1.7159	232.86

$T = 373 \text{ K}$

0.1	995.62	790.01	1955.54	1492.73	1280.54	1672.88	1276.97	0.7655	285.42
10	1066.09	802.12	1933.51	1496.76	1153.63	1417.01	1096.93	0.8141	293.67
50	1281.41	838.86	1892.62	1513.32	880.06	907.96	726.00	0.9693	311.54
100	1475.20	871.36	1877.40	1533.64	720.02	645.56	527.35	1.1153	316.02
120	1540.07	882.10	1875.47	1541.30	677.96	581.60	477.97	1.1657	314.80
150	1628.29	896.58	1874.88	1552.31	627.66	508.09	420.67	1.2353	310.78
180	1707.99	909.56	1876.14	1562.81	587.95	452.43	376.87	1.2995	304.72

210	1781.01	921.36	1878.61	1572.85	555.58	408.68	342.17	1.3594	297.07
240	1848.62	932.22	1881.91	1582.47	528.55	373.29	313.90	1.4159	288.13
270	1911.74	942.29	1885.81	1591.73	505.55	344.02	290.37	1.4695	278.13
300	1971.06	951.70	1890.13	1600.66	485.67	319.37	270.46	1.5207	267.23
330	2027.11	960.56	1894.76	1609.29	468.28	298.29	253.35	1.5699	255.56
360	2080.32	968.92	1899.62	1617.65	452.91	280.05	238.48	1.6172	243.23
390	2131.02	976.85	1904.65	1625.75	439.20	264.09	225.42	1.6631	230.32

$T = 383 \text{ K}$

0.1	956.25	779.80	1991.89	1523.88	1321.65	1833.12	1402.42	0.7210	276.04
10	1030.37	792.81	1966.78	1526.77	1180.67	1530.46	1188.06	0.7714	285.46
50	1252.98	831.50	1921.34	1543.10	885.01	953.81	766.04	0.9279	305.37
100	1450.73	865.12	1904.42	1563.12	718.24	669.15	549.23	1.0734	311.10
120	1516.62	876.15	1902.11	1570.69	674.97	600.91	496.21	1.1232	310.20
150	1606.06	891.00	1901.12	1581.60	623.51	523.01	435.11	1.1921	306.59
180	1686.73	904.26	1902.07	1592.00	583.07	464.41	388.70	1.2555	300.86
210	1760.55	916.29	1904.29	1601.95	550.23	418.56	352.11	1.3146	293.48
240	1828.83	927.33	1907.39	1611.50	522.88	381.62	322.42	1.3702	284.77
270	1892.53	937.57	1911.11	1620.68	499.66	351.16	297.79	1.4229	274.97
300	1952.36	947.13	1915.27	1629.53	479.64	325.57	277.00	1.4732	264.25
330	2008.86	956.10	1919.76	1638.08	462.15	303.74	259.18	1.5215	252.74
360	2062.48	964.57	1924.49	1646.36	446.71	284.89	243.72	1.5680	240.55
390	2113.55	972.61	1929.40	1654.39	432.96	268.42	230.16	1.6130	227.77

$T = 398 \text{ K}$

10	977.92	778.65	2018.05	1572.06	1226.44	1723.88	1342.91	0.7114	273.15
50	1211.74	820.49	1964.98	1587.79	893.75	1027.25	830.06	0.8700	296.28
100	1415.36	855.87	1945.22	1607.20	716.32	705.92	583.26	1.0147	303.86
120	1482.75	867.36	1942.29	1614.60	671.19	630.83	524.40	1.0640	303.46
150	1573.98	882.75	1940.59	1625.28	617.92	545.97	457.26	1.1318	300.45
180	1656.06	896.44	1941.00	1635.48	576.36	482.73	406.75	1.1940	295.20

210	1731.05	908.82	1942.79	1645.23	542.79	433.61	367.20	1.2518	288.21
240	1800.32	920.16	1945.52	1654.59	514.96	394.26	335.30	1.3061	279.84
270	1864.87	930.64	1948.91	1663.59	491.41	361.96	308.97	1.3576	270.33
300	1925.45	940.41	1952.77	1672.27	471.16	334.94	286.83	1.4067	259.87
330	1982.62	949.57	1956.98	1680.65	453.52	311.96	267.91	1.4537	248.59
360	2036.84	958.21	1961.46	1688.76	437.98	292.17	251.55	1.4990	236.61
390	2088.46	966.39	1966.13	1696.63	424.16	274.93	237.25	1.5428	224.03

$T = 403 \text{ K}$

10	960.73	773.87	2035.53	1587.27	1243.15	1795.37	1400.00	0.6924	269.05
50	1198.35	816.83	1979.67	1602.68	897.03	1053.04	852.51	0.8518	293.29
100	1403.91	852.82	1958.89	1621.85	715.89	718.56	594.93	0.9963	301.50
120	1471.80	864.46	1955.73	1629.18	670.11	641.06	534.02	1.0453	301.27
150	1563.61	880.04	1953.77	1639.76	616.23	553.78	464.78	1.1128	298.45
180	1646.16	893.87	1953.99	1649.87	574.29	488.94	412.84	1.1746	293.35
210	1721.53	906.37	1955.61	1659.54	540.48	438.70	372.28	1.2320	286.50
240	1791.12	917.80	1958.19	1668.82	512.48	398.52	339.63	1.2860	278.24
270	1855.95	928.37	1961.45	1677.74	488.82	365.60	312.71	1.3370	268.83
300	1916.77	938.21	1965.20	1686.34	468.49	338.08	290.11	1.3857	258.45
330	1974.16	947.43	1969.31	1694.65	450.79	314.72	270.82	1.4324	247.25
360	2028.58	956.12	1973.68	1702.69	435.21	294.61	254.16	1.4773	235.34
390	2080.38	964.35	1978.26	1710.49	421.37	277.10	239.60	1.5206	222.81

$T = 423 \text{ K}$

10	893.40	754.37	2107.49	1648.78	1317.83	2122.90	1660.83	0.6208	252.58
50	1146.58	802.21	2039.14	1662.08	912.07	1163.32	948.21	0.7840	281.64
100	1359.78	840.72	2013.82	1680.02	715.25	771.11	643.29	0.9276	292.36
120	1429.60	853.01	2009.66	1686.98	666.81	683.33	573.61	0.9758	292.78
150	1523.71	869.33	2006.53	1697.07	610.39	585.81	495.46	1.0419	290.74
180	1608.07	883.75	2005.82	1706.72	566.89	514.27	437.58	1.1023	286.28
210	1684.93	896.72	2006.68	1715.97	532.06	459.36	392.81	1.1583	279.95

240	1755.78	908.55	2008.59	1724.84	503.39	415.77	357.03	1.2107	272.14
270	1821.71	919.44	2011.25	1733.37	479.26	380.27	327.73	1.2603	263.11
300	1883.49	929.57	2014.45	1741.58	458.61	350.76	303.24	1.3075	253.07
330	1941.73	939.04	2018.04	1749.52	440.69	325.80	282.45	1.3527	242.17
360	1996.91	947.95	2021.93	1757.20	424.96	304.40	264.54	1.3961	230.54
390	2049.42	956.38	2026.05	1764.65	411.01	285.83	248.95	1.4380	218.26

$T = 448 \text{ K}$

10	812.42	728.94	2202.17	1727.46	1430.59	2649.66	2078.49	0.5399	231.88
50	1085.71	783.90	2114.57	1735.31	935.49	1318.74	1082.22	0.7094	267.80
100	1308.21	825.81	2082.51	1751.05	717.04	841.51	707.57	0.8521	281.74
120	1380.34	838.92	2076.82	1757.36	665.04	739.33	625.61	0.8995	282.98
150	1477.20	856.22	2071.90	1766.56	605.25	627.74	535.23	0.9642	281.95
180	1563.73	871.39	2069.77	1775.40	559.70	547.13	469.31	1.0230	278.30
210	1642.37	884.97	2069.41	1783.88	523.55	485.98	418.92	1.0773	272.64
240	1714.72	897.29	2070.25	1792.01	493.99	437.89	379.03	1.1281	265.40
270	1781.94	908.61	2071.93	1799.84	469.25	399.01	346.61	1.1760	256.87
300	1844.86	919.09	2074.23	1807.37	448.17	366.88	319.68	1.2216	247.26
330	1904.12	928.88	2076.98	1814.65	429.94	339.85	296.93	1.2651	236.75
360	1960.22	938.06	2080.07	1821.69	413.98	316.78	277.43	1.3068	225.47
390	2013.55	946.73	2083.42	1828.52	399.88	296.84	260.52	1.3471	213.50

$T = 473 \text{ K}$

10	734.98	702.03	2301.72	1808.03	1568.35	3356.89	2636.88	0.4672	210.99
50	1028.95	765.47	2189.72	1805.59	964.49	1496.41	1233.91	0.6445	254.86
100	1260.40	811.05	2149.52	1818.26	721.92	917.53	776.13	0.7868	272.16
120	1334.74	825.05	2141.97	1823.67	666.07	799.09	680.35	0.8335	274.26
150	1434.18	843.35	2134.86	1831.66	602.69	671.90	576.47	0.8970	274.28
180	1522.76	859.30	2130.95	1839.38	554.95	581.43	501.87	0.9545	271.46
210	1603.06	873.49	2129.06	1846.81	517.39	513.58	445.49	1.0074	266.51
240	1676.83	886.32	2128.54	1853.94	486.88	460.70	401.27	1.0568	259.88

270	1745.26	898.06	2128.98	1860.80	461.48	418.26	365.57	1.1033	251.88
300	1809.24	908.91	2130.11	1867.41	439.93	383.40	336.11	1.1475	242.75
330	1869.44	919.01	2131.77	1873.79	421.36	354.22	311.35	1.1896	232.66
360	1926.39	928.48	2133.83	1879.97	405.15	329.42	290.23	1.2299	221.75
390	1980.49	937.39	2136.20	1885.97	390.86	308.06	271.98	1.2687	210.12

^aRelative expanded uncertainties ($k = 2$) at 95 % confidence of : density, $U(\rho) = 0.2\%$; isobaric specific heat capacity, $U(C_p) = 2.2\%$; isochoric specific heat capacity, $U(C_v) = 2.6\%$; isobaric expansivity, $U(\alpha_p) = 1\%$; isothermal compressibility, $U(\beta_T) = 0.6\%$; isentropic compressibility, $U(\beta_s) = 0.2\%$; thermal pressure coefficient, $U(p_c) = 1\%$; internal pressure, $U(p_{int}) = 2.7\%$. ^b Sound-speed values calculated using correlations from Eq. (1) and Eq. (2).

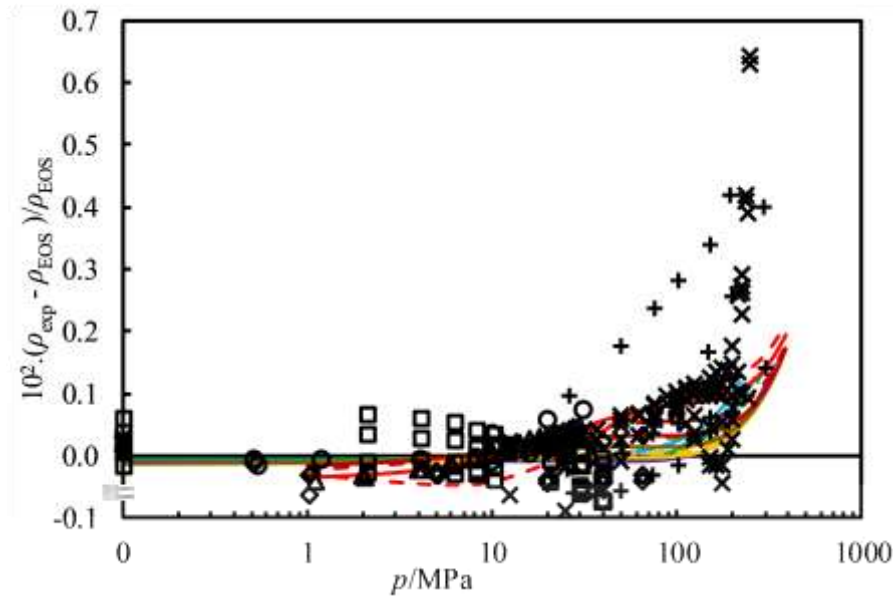


Fig. 7. Deviations from the Helmholtz EOS of Lemmon and Span [3] of liquid densities of toluene, ρ_{exp} , as a function of pressure at various temperatures. Derived in this work ($u(\rho) = 0.20\%$, $k = 2$) (solid and dotted lines): —, $T = 283$ K; —, $T = 298$ K; —, $T = 306$ K; —, $T = 321$ K; —, $T = 343$ K; —, $T = 348$ K; —, $T = 363$ K; —, $T = 373$ K; —, $T = 383$ K; —, $T = 398$ K; —, $T = 403$ K; —, $T = 423$ K; —, $T = 448$ K; —, $T = 473$ K. Literature data (experimental): \square , Moravkova *et al.* [31] from 298.15 K to 328.15 K; \triangle , Sommer *et al.* [32] at 453.15 K and 473.15 K; \times , Kashiwagi *et al.* [33] between 273.15 K and 373.12 K; $+$, Dymond *et al.* [34] between 298.23 K and 373.27 K; \circ , McLinden & Splett [23] between 283.15 K and 473.16 K; \diamond , Tay & Trusler [20] between 283.16 K and 473.15 K.

7. Comparison of derived properties with literature data

The derived density ρ , isobaric heat capacity C_p , isobaric expansivity α_p , isothermal compressibility β_T and isochoric heat capacity C_v obtained by means of thermodynamic integration and relations described in the previous section were compared against the values obtained from Helmholtz EOS of Lemmon and Span [3] and literature data, with the EOS as the baseline. Although there is a great amount of experimental data available for density of liquid toluene in our temperature and pressure range, experimental data of other thermodynamic properties are limited. Therefore, comparisons against the derived thermodynamic properties data reported in literature are also provided where necessary.

All comparisons are made at isotherms near the average experimental temperatures as functions of pressure. **Fig. 7** shows the relative percentage deviation of derived density and literature data against the EOS. The deviations increase with increasing isotherms with lowest deviations observed at the lowest pressures. Most of our derived density values lie within the reported uncertainty of 0.05 % of the EOS up to 100 MPa and within the reported uncertainty of 0.5 % of the EOS at higher pressures. Average deviations of our data against the EOS are $AARD = 0.05\%$ with maximum deviation, $MARD = 0.2\%$ over the entire pressure range. These results suggest very close agreement between our derived data and the EOS prediction for density, mainly due to the high-quality fits of sound-speed and density at reference isobar.

The deviations in density of Kashiwagi *et al.* [33] between $T = (273.15 \text{ and } 373.14) \text{ K}$ and $p = (0.1 \text{ and } 250) \text{ MPa}$ are up to 0.6 % from the EOS. The data of Dymond *et al.* [34] between temperatures of 298.23 K to 373.27 K and pressures up to 300 MPa are at a maximum of 0.4 %. More recent data of Morávková *et al.* [31], McLinden & Splett [23], Sommer *et al.* [32] and Tay & Trusler [20] show better agreement with the EOS with maximum deviations in the experimental range of this work of 0.08 %, 0.07 %, 0.05 % and 0.06 %, respectively.

Similarly, the derived isobaric heat capacity is compared against the EOS and available experimental and derived data from the literature as shown in **Fig. 8**. The derived values are in close agreement with the EOS with $AARD = 0.5\%$ and $MARD = 1.5\%$. The highest deviations generally occur at the highest pressures and lowest temperatures. All derived values fall within the reported experimental uncertainty of the EOS, which is reported to be up to 3 %. The experimental data of Shulga *et al.* [35] at $T = (326.20,$

354.50 and 401.50) K and pressures up to 54 MPa deviate by up to 1.3 % from the EOS. Similarly, the data of Akhundov *et al.* [24] between 298.14 K and 473.11 K and pressures up to 20 MPa vary from the EOS by up to 0.7 %. The data of Segovia *et al.* [36] at 313.15 K and 333.15 K and pressures up to 30 MPa vary from the EOS by up to 0.9 %.

Our derived isobaric expansivity values compared against the EOS indicate maximum deviations of nearly 3 % occurring at the lowest pressures of the highest temperatures as shown in **Fig. 9**. The experimental data for isobaric expansivity of liquid toluene of Chorazewski *et al.* [37] between $T = (304.1 \text{ and } 422.2) \text{ K}$ and pressures up to 195 MPa deviate from the EOS by as much as 8.6 %. The experimental data of Navia *et al.* [38] between $T = (308.15 \text{ and } 348.15) \text{ K}$ and pressures up to 55 MPa are in much closer agreement with the EOS. The average deviations of their data are nearly 0.5 % with maximum deviations of 1.4 %. Both these experimental data sets have reported uncertainty of 2 %.

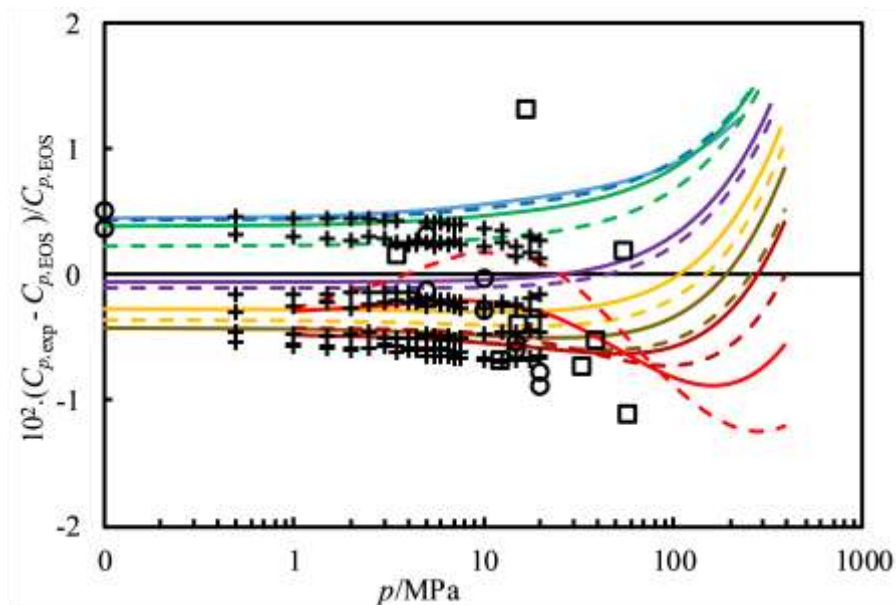


Fig. 8. Deviations from the Helmholtz EOS of Lemmon and Span [3] of liquid isobaric heat capacities of toluene, $C_{p,\text{exp}}$, as a function of pressure at various temperatures. Derived in this work ($u(C_p) = 2.2 \%$, $k = 2$) (solid and dotted lines): —, $T = 283 \text{ K}$; —•—, $T = 298 \text{ K}$; —•—, $T = 306 \text{ K}$; —•—, $T = 321 \text{ K}$; —•—, $T = 343 \text{ K}$; —•—, $T = 348 \text{ K}$; —•—, $T = 363 \text{ K}$; —•—, $T = 373 \text{ K}$; —•—, $T = 383 \text{ K}$; —•—, $T = 398 \text{ K}$; —•—, $T = 403 \text{ K}$; —•—, $T = 423 \text{ K}$; —•—, $T = 448 \text{ K}$; —•—, $T = 473 \text{ K}$. Literature data (experimental): □, Shulga *et al.* [35] at 326.20 K, 354.50 K and 401.50 K; +, Akhundov & Eksaev [24] between 298.14 K to 473.11 K; ○, Segovia *et al.* [36] at 313.15 K and 333.15 K.

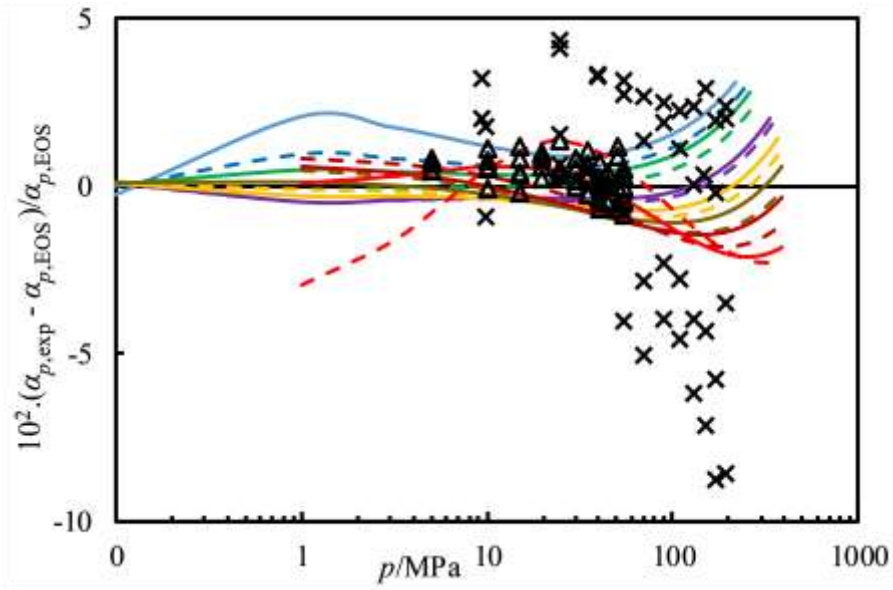


Fig. 9. Deviations from the Helmholtz EOS of Lemmon and Span [3] of liquid isobaric expansivities of toluene, $\alpha_{p,\text{exp}}$, as a function of pressure at various temperatures. Derived in this work ($u(p) = 0.60\%$, $k = 2$) (solid and dotted lines): --- , $T = 283$ K; --- , $T = 298$ K; --- , $T = 306$ K; --- , $T = 321$ K; --- , $T = 343$ K; --- , $T = 348$ K; --- , $T = 363$ K; --- , $T = 373$ K; --- , $T = 383$ K; --- , $T = 398$ K; --- , $T = 403$ K; --- , $T = 423$ K; --- , $T = 448$ K; --- , $T = 473$ K. Literature data (experimental): \times , Chorazewski *et al.* [37] between $T = (304.1 \text{ and } 422.2)$ K; \triangle , Navia *et al.* [38] between $T = (308.15 \text{ and } 348.15)$ K.

Fig. 10 shows comparison between our derived isochoric heat capacity values against the EOS with $AARD = 0.5\%$ and $MARD = 1.5\%$. Experimental data of isochoric heat capacity values for our range of study is not currently available in literature. Therefore, comparisons of derived values from literature against the EOS are provided. The deviations of values obtained from non-analytical EOS of Goodwin [22] against the Helmholtz EOS at $T = (320, 400 \text{ and } 470)$ K and at pressures up to 100 MPa are up to 3% with the highest deviations occurring at highest pressures. Similarly, the derived data of Sun *et al.* [39] obtained from sound-speed data at 320 K and pressures up to 60 MPa show maximum deviations of up to 0.17%. At that temperature and pressure range, our data indicate maximum deviations of nearly 0.3% against the Helmholtz EOS. The derived data Shchamialiou *et al.* [18] between $T = (313.15 \text{ and } 413.15)$ K and pressures up to 60 MPa vary by up to 0.5% from the EOS.

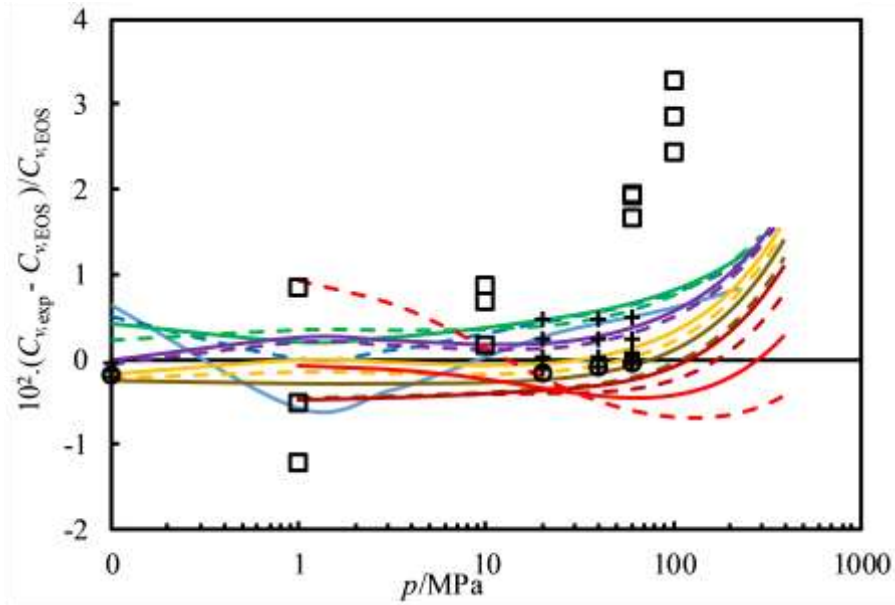


Fig. 10. Deviations from the Helmholtz EOS of Lemmon and Span [3] of liquid isochoric heat capacities of toluene, $C_{v,exp}$, as a function of pressure at various temperatures. Derived in this work ($u(C_v) = 2.6\%$, $k = 2$) (solid lines): --- , $T = 283$ K; --- , $T = 298$ K; --- , $T = 306$ K; --- , $T = 321$ K; --- , $T = 343$ K; --- , $T = 348$ K; --- , $T = 363$ K; --- , $T = 373$ K; --- , $T = 383$ K; --- , $T = 398$ K; --- , $T = 403$ K; --- , $T = 423$ K; --- , $T = 448$ K; --- , $T = 473$ K. Literature data (all reported as derived values): \square , EOS of Goodwin [22] at 320 K, 400 K and 470 K; \circ , Sun *et al.* [39] at 320 K; + , Shchamialiou *et al.* [18] between $T = (313.15$ and $413.15)$ K.

Additionally, the derived isothermal compressibility values of liquid toluene are compared against the Helmholtz EOS as shown in **Fig. 11**. Deviations from the EOS of our derived data are $AARD = 1\%$ and $MARD = 3.5\%$. Derived values of isothermal compressibility available in the literature are also compared against the EOS. The data of Eastel *et al.* [40] between $T = (278.15$ and $323.14)$ K at pressures up to 275 MPa show very high deviations of up to 44% when compared to the EOS. These very high deviations occur at the highest pressures. For clarity, the highest deviations of this data set is not included in **Fig. 11**. The derived isothermal compressibility of Shchamialiou *et al.* [18] between $T = (313.15$ and $413.15)$ K and pressures up to 60 MPa vary by up to 0.9% from the EOS.

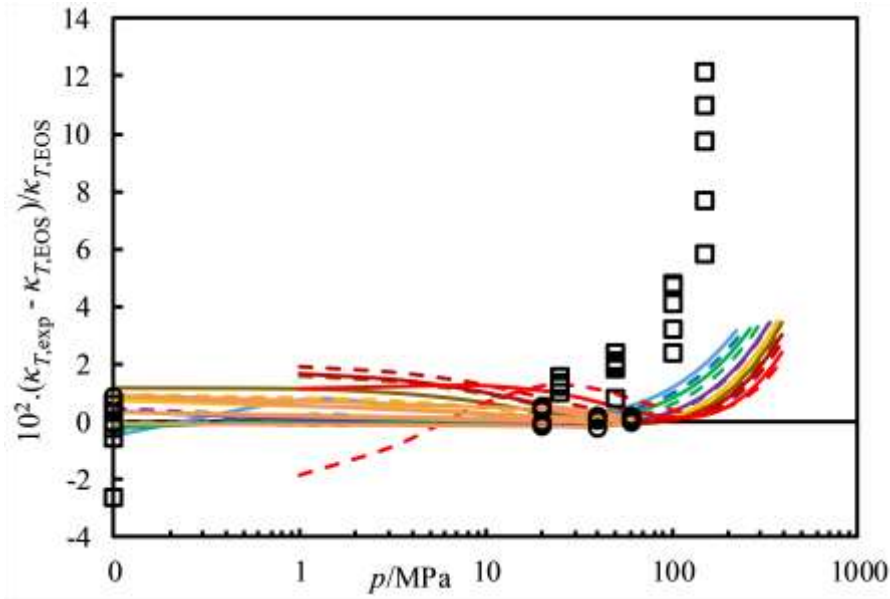


Fig. 11. Deviations from the Helmholtz EOS of Lemmon and Span [3] of liquid isothermal compressibilities of toluene, $\kappa_{T,exp}$, as a function of pressure at various temperatures. Derived in this work ($u(\tau) = 0.28\%$, $k = 2$) (solid and dotted lines): —, $T = 283$ K; —■, $T = 298$ K; —■, $T = 306$ K; ■, $T = 321$ K; —■, $T = 343$ K; ■, $T = 348$ K; —■, $T = 363$ K; —■, $T = 373$ K; —■, $T = 383$ K; ■, $T = 398$ K; —■, $T = 403$ K; ■, $T = 423$ K; —■, $T = 448$ K; ■, $T = 473$ K. Literature data (all reported as derived values): □, Eastel *et al.* [40] between $T = (278.15$ and $323.14)$ K; ○, Shchamialiou *et al.* [18] between $T = (313.15$ and $413.15)$ K.

8. Conclusions

Accurate measurements of the speed-of-sound of liquid toluene from temperature range between 283.15 K to 473.15 K were carried out at pressures up to 390 MPa using double-path pulse-echo method independently at UWA and ICL. A comparison of the resulting data with the most accurate literature data available to date along with three equation-of-state models was carried out. The standard uncertainties of our experimental data are at most 0.06 %, which fall well within the reported EOS uncertainty of 2 %. Comparison with recent and most accurate literature data shows good agreement, with maximum deviations of up to 0.08 % suggesting that the recent sound-speed data will be useful for future retuning of the EOS along with additional thermophysical property data such as density and VLE. By employing the method of thermodynamic integration, a range of thermodynamic properties were derived and compared against the existing literature experimental and derived data as well as the Helmholtz EOS. Our derived properties show better agreement with the EOS within the range of uncertainties as compared to the most experimental and derived properties. Additionally, a comprehensive error propagation analysis was carried out and uncertainties of derived properties were

empirically evaluated using a method previously employed for pure water. Temperature derivatives of perturbations were evaluated by employing sum-of-sine fit to capture accurate dynamic fluctuations of the perturbations in derived properties. Finally, we suggest that the derived properties obtained here from the highly accurate sound-speed measurements along with more recent accurate literature data could potentially be used to improve the predictions of the EOS.

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